



The electrical supply chain of the future will incorporate a higher percentage of renewable energy (i.e. wind and PV solar). While clean and unlimited, these forms of energy are intermittent in nature and will require some form of energy storage to meet their potential. Thermal storage is not only an easy way to store energy but it is reemerging as a valuable energy and energy cost saving technology for building owners.

(IR) Ingersoll Rand

We'll cover a bit of theory and application, then demonstrate the design steps for a small ice storage system from layout to operation and control. We'll discuss how to make it affordable, expose hidden costs in energy tariffs which raise ROI, and identify and address the most common stumbling blocks.

By attending this ENL you will be able to:

- 1. Provide a clear understanding of how an ice storage system operates
- 2. Provide an economic rationale for ice storage
- 3. Dispel common myths about ice storage
- 4. Understand how to avoid the most common stumbling blocks

Agenda

- 1) Opening (welcome, agenda, introductions)
- 2) Why ice storage
 - a) Electrical infrastructure
 - b) Economics
 - c) Environmental stewardship
 - d) Myths about ice storage
- 3) Typical applications
- 4) Electricity rate introduction
- 5) Design overview
 - a) Partial versus full
 - b) Influences driving partial storage
 - c) Influences driving full storage
 - d) Considerations
- 6) Controls
- 4) Economic summary





Trane Engineers Newsletter Live Series Ice Storage Design and Application (2009)

Susanna Hanson | applications engineer | Trane

Susanna is an applications engineer at Trane with over eleven years of experience with chilled-water systems and HVAC building load and energy analysis. Her primary responsibility is to aid system design engineers and Trane personnel in the proper design and application of HVAC systems. Her main areas of expertise include chilled-water systems and ASHRAE Standard 90.1. She is also a Certified Energy Manager.

She has authored several articles on chilled water plant design, and is a member of ASHRAE SSPC 90.1 Energy Standard for Buildings Except Low-Rise Residential Buildings. Susanna earned a bachelor's degree in industrial and systems engineering from the University of Florida, where she focused on building energy management and simulation.

Lee Cline | senior systems engineer | Trane

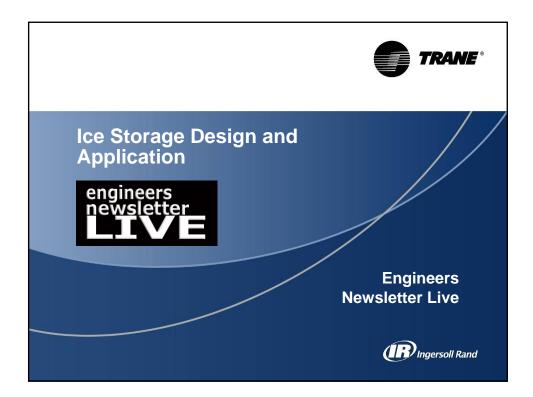
Lee is an engineer in the Systems Engineering Department with over 28 years experience at Trane. His career at Trane started as a factory service engineer for heavy refrigeration, helping to introduce the CVHE centrifugal chiller with electronic controls to the industry. Following that Lee was a member of the team that kicked off the microelectronic building automation and Integrated Comfort Systems controls – ICS – offering at Trane. He continues to push new unit and system control and optimization concepts into the industry. As a Systems Engineer Lee also has the opportunity to discuss HVAC system application and control with owners, engineers and contractors on a daily basis.

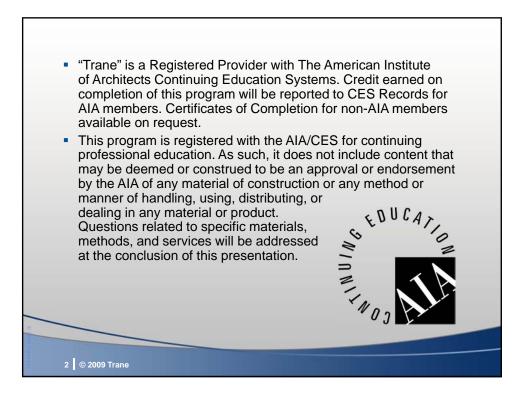
Lee has a Bachelors degree in Mechanical Engineering from Michigan Technological University. He is a Registered Professional Engineer in the State of Wisconsin.

Paul Valenta | Vice-President Sales and Marketing | CALMAC Mfg. Corp.

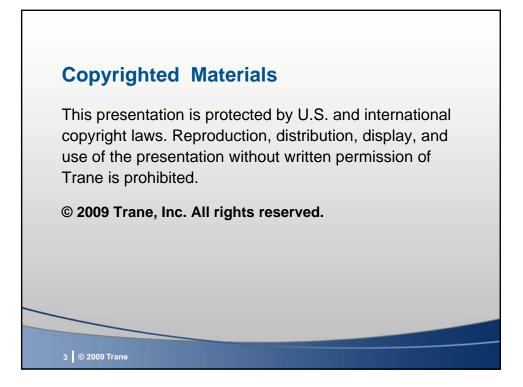
Paul is a vice-president at CALMAC Manufacturing Corporation with over 20 years experience in the ice energy field. CALMAC celebrated its 60th birthday in 2008 and has a long history of providing valuable energy saving products. Paul's career at CALMAC started as a regional sales manager responsible for sales and distribution of ice storage systems in the Midwest. Without utility incentives and off peak rates, Paul specialized in developing partial ice energy storage applications in schools and offices and demonstrating their viability with life cycle costs. He has been involved in several hundred ice storage projects all over the world. Currently Paul is Marketing and Sales Manager for CALMAC. He has authored several articles on ice energy storage and rightsizing cooling plants with energy storage, is a member or ASHRAE and is a LEED Accredited Professional. Paul has a degree in Electrical Engineering from the University of Nebraska.















Today's Presenters



Paul Valenta Calmac National Sales Manager

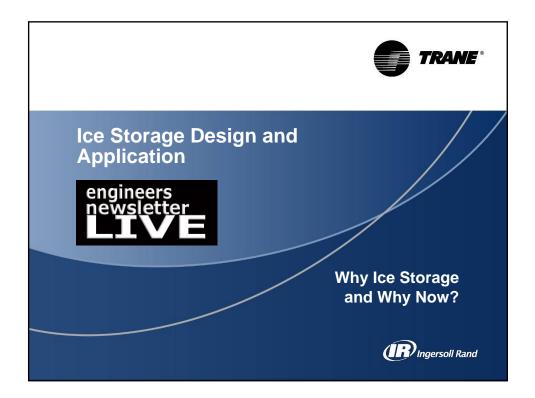
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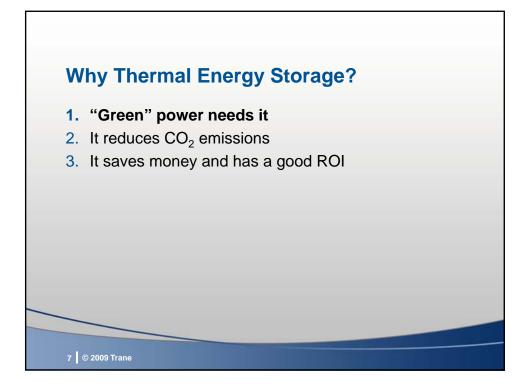
Susanna Hanson Applications Engineer

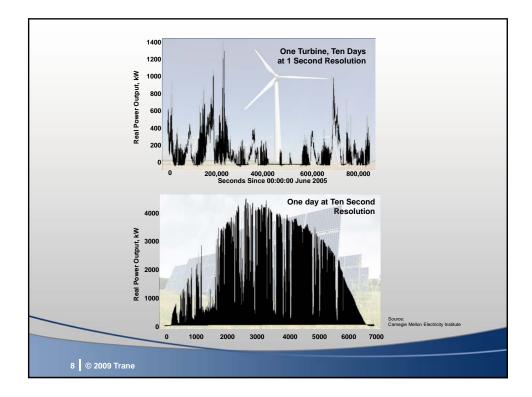


Lee Cline Systems Engineer

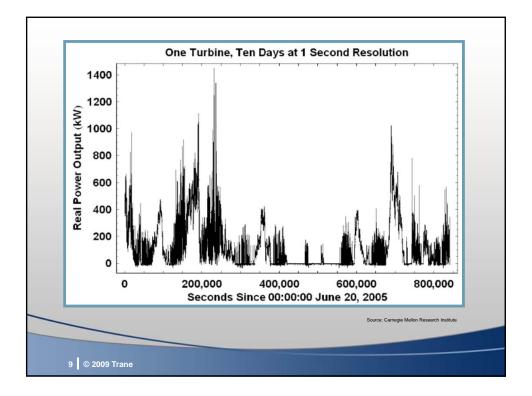


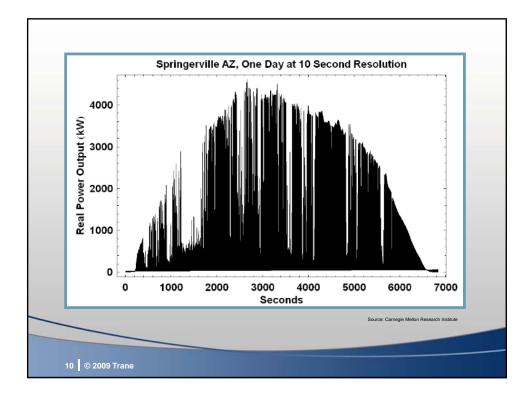




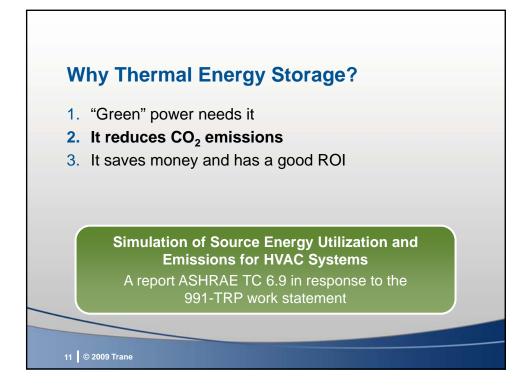


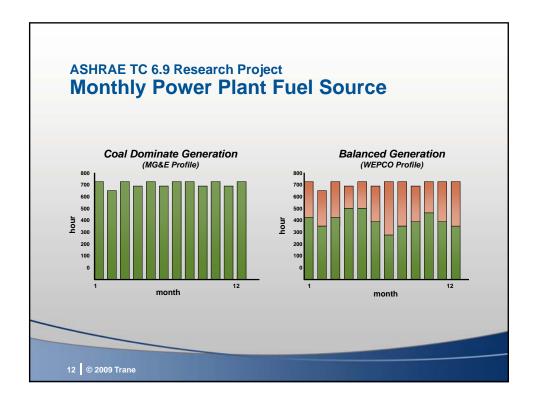






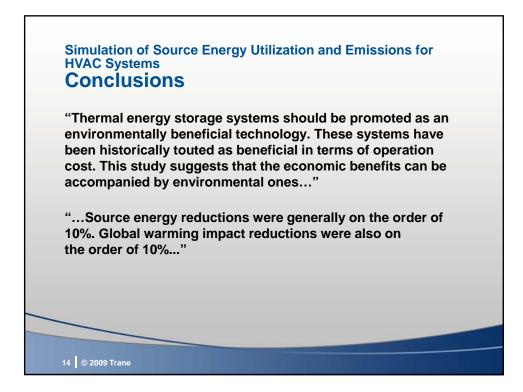




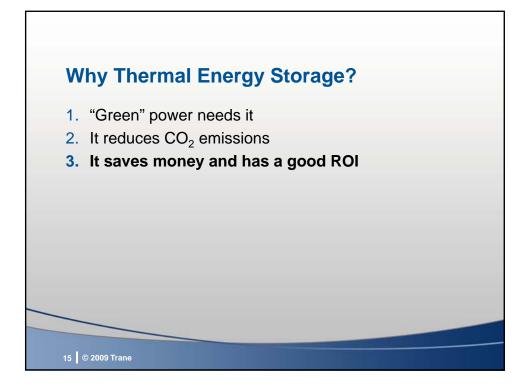


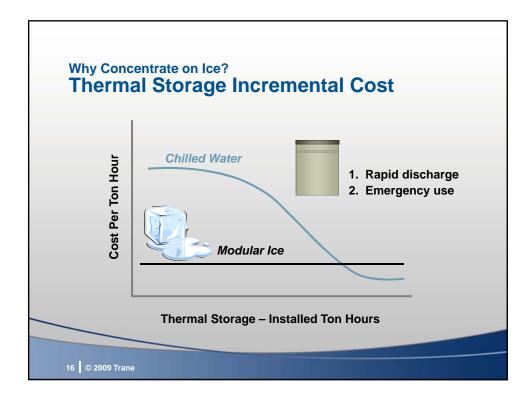


		Dominant eration Pro	•	Coal/Natural Gas Utility Generation Profile				
System	Site Electricity (% of base)	Source Energy (% of base)	CO ₂ Emission (% of base)	Site Electricity (% of base)	Source Energy (% of base)	CO ₂ Emission (% of base)		
Electric Chiller (base)	100%	100%	100%	100%	100%	100%		
Office Ice Storage	86%	86%	86%	86%	86%	86%		
School W/C—Ice	88%	88%	87%	88%	88%	88%		
School A/C—Ice	87%	87%	86%	87%	87%	88%		

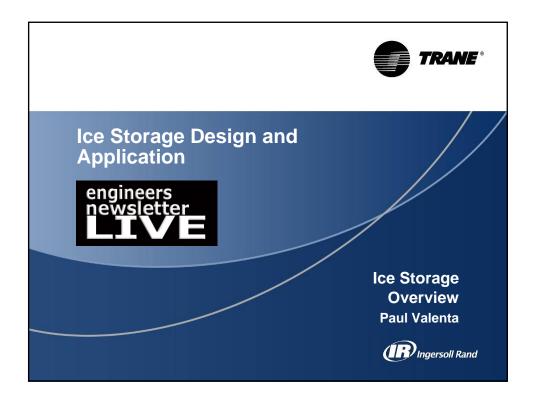


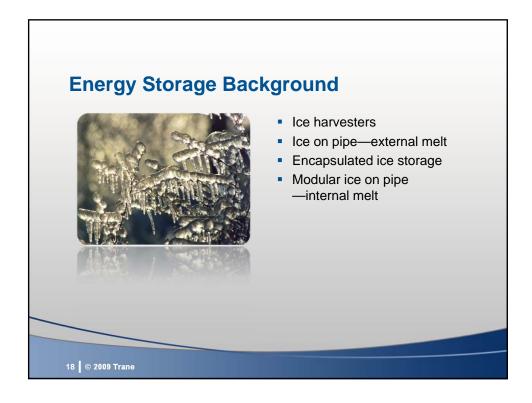




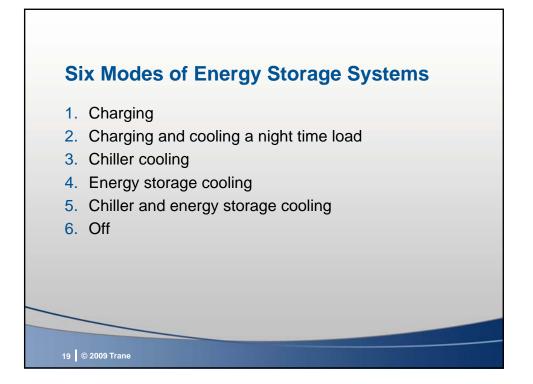


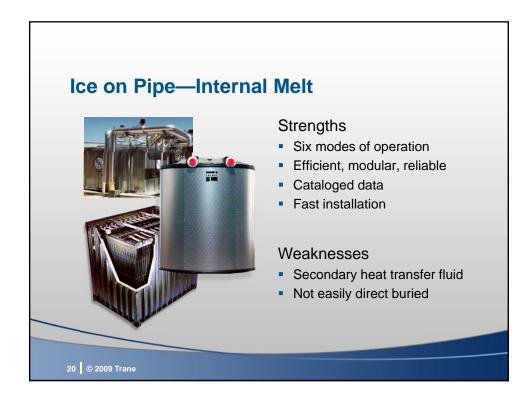




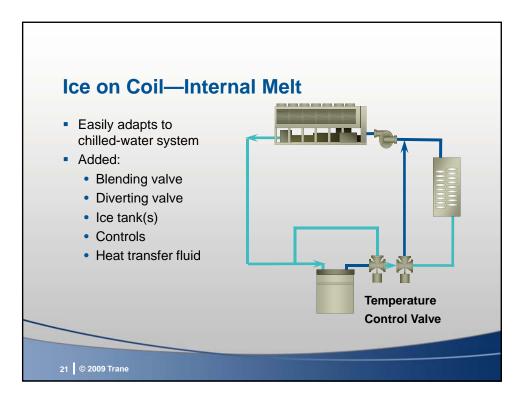


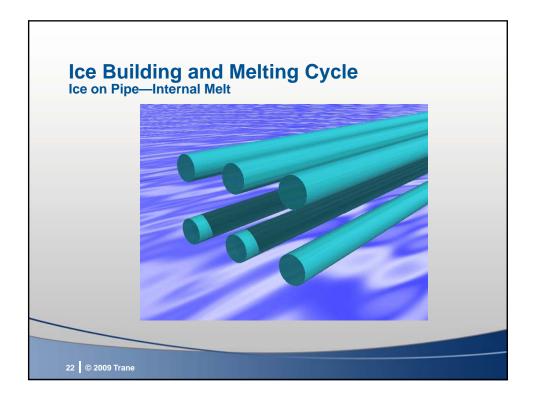




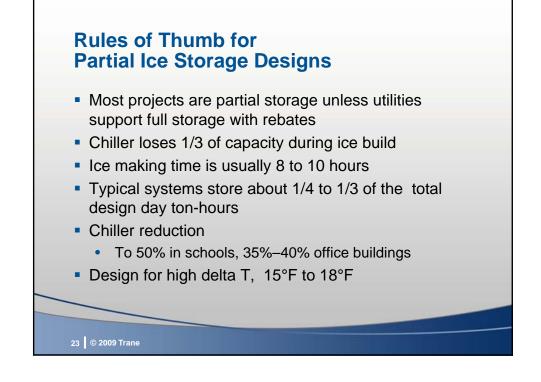






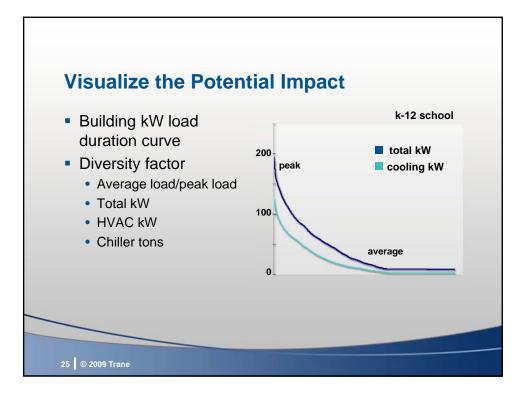






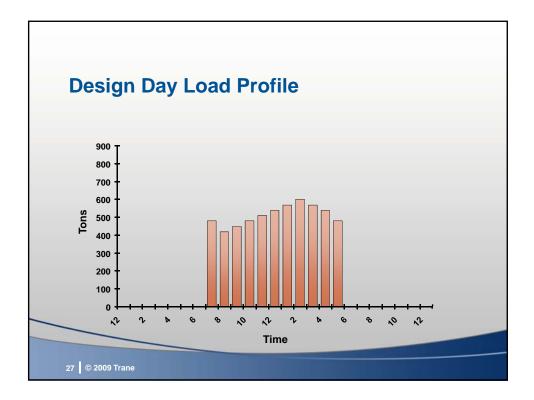


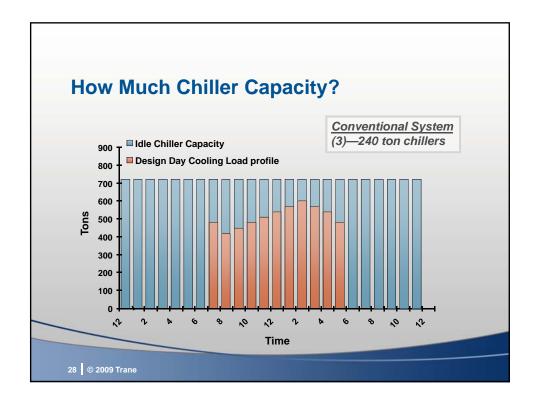




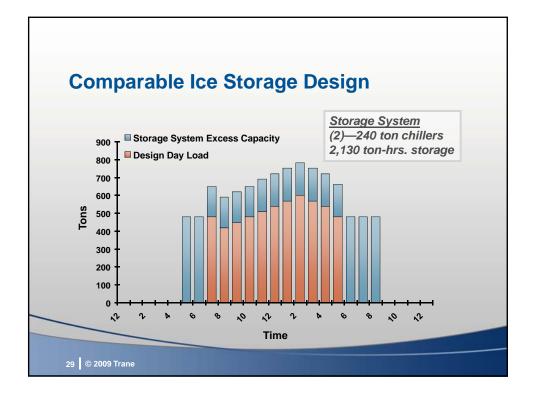


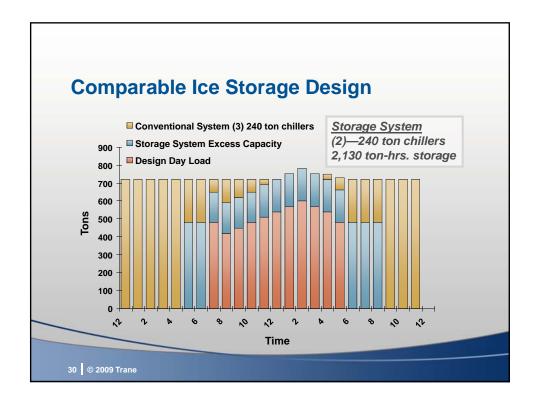




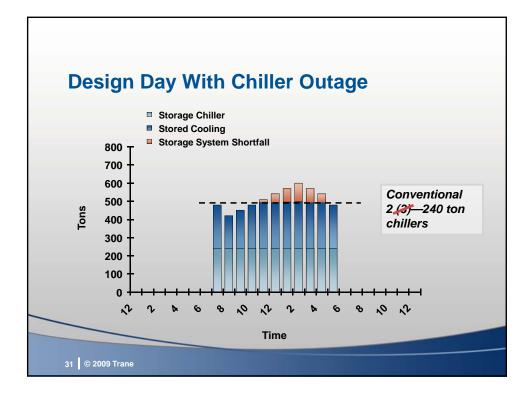


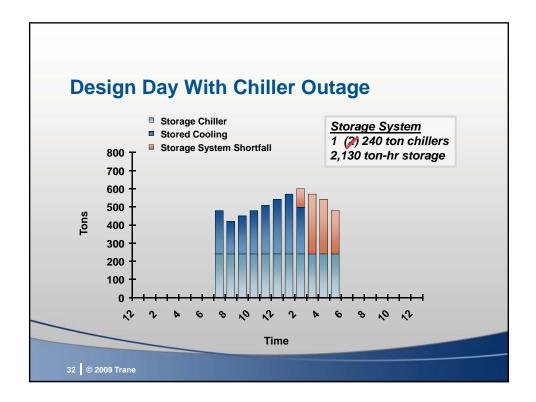




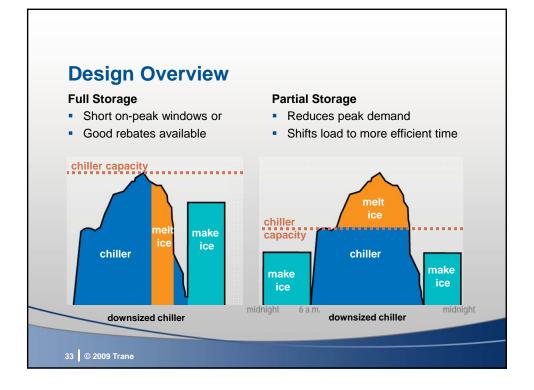


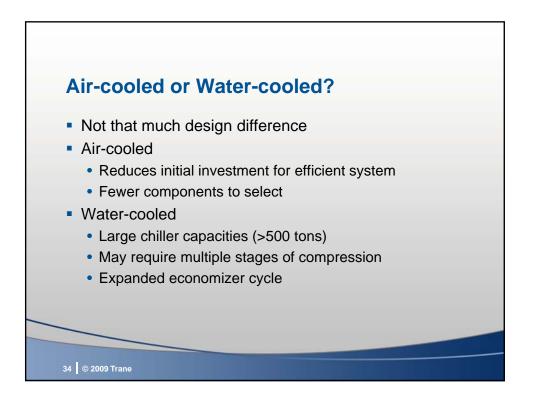




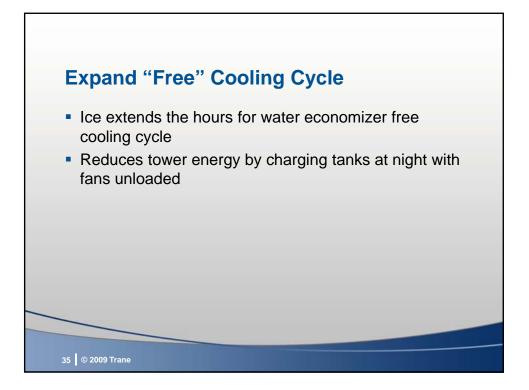


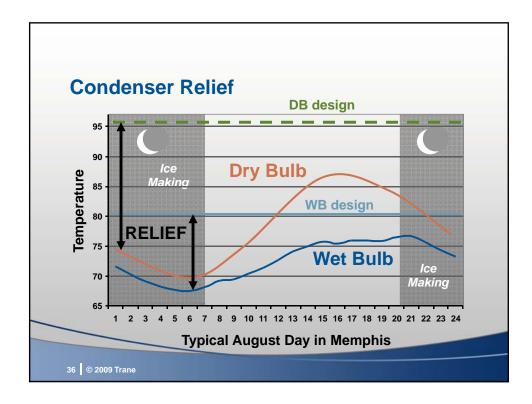




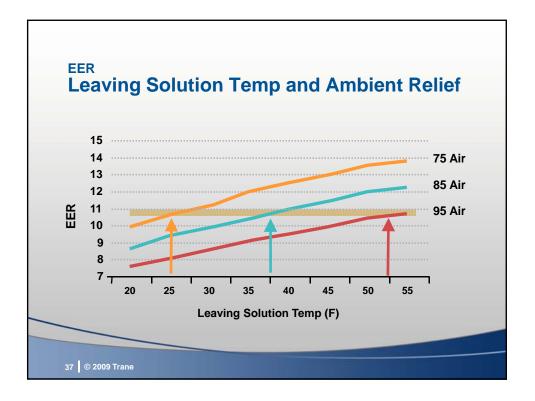


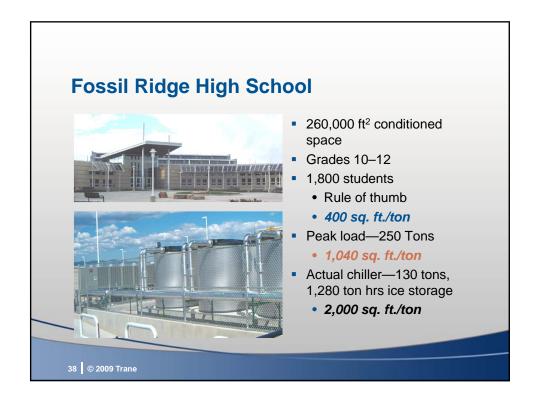




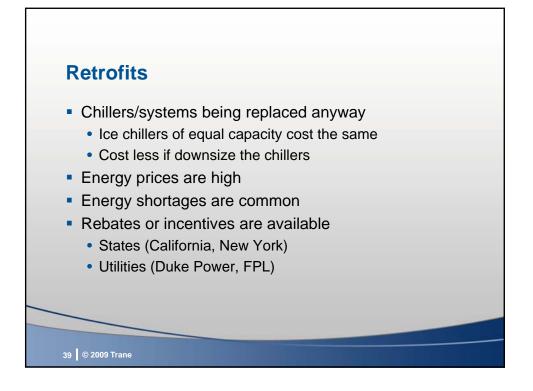


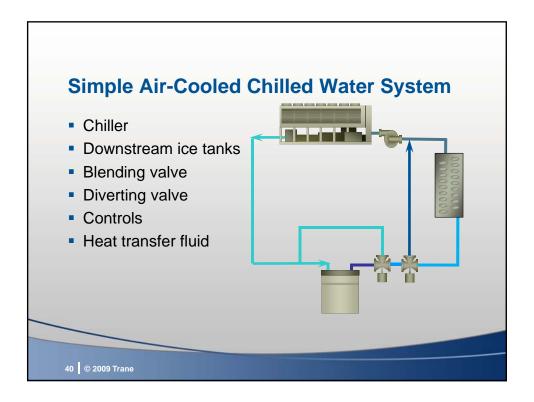




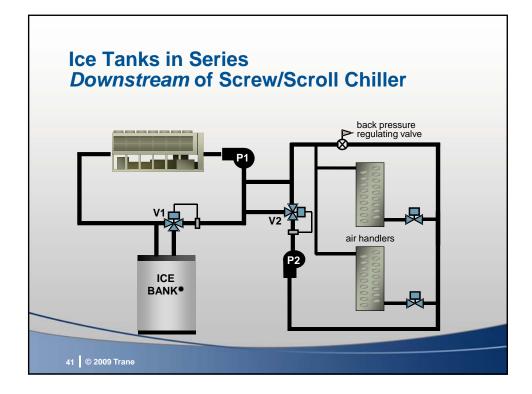


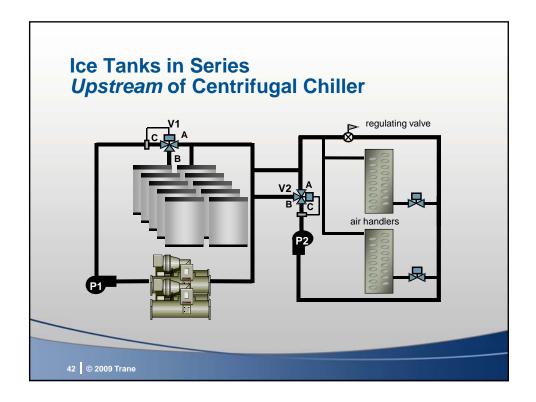




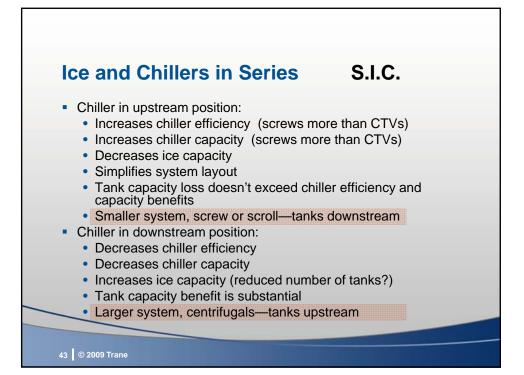


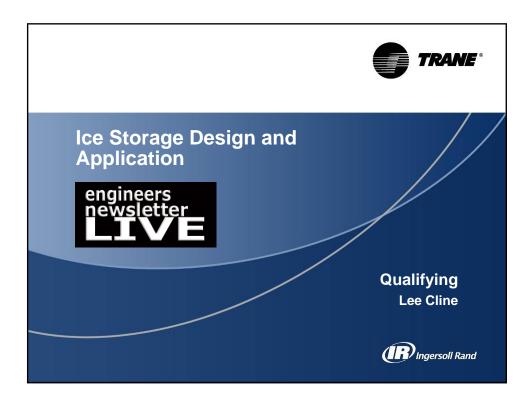




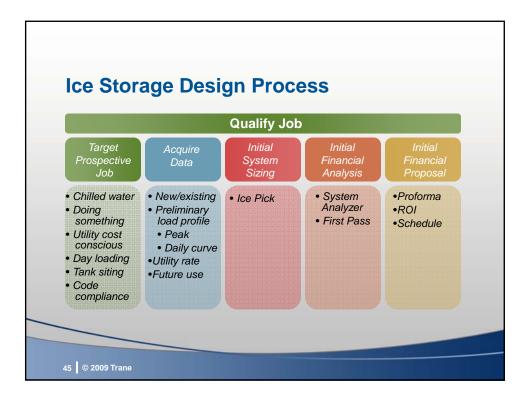


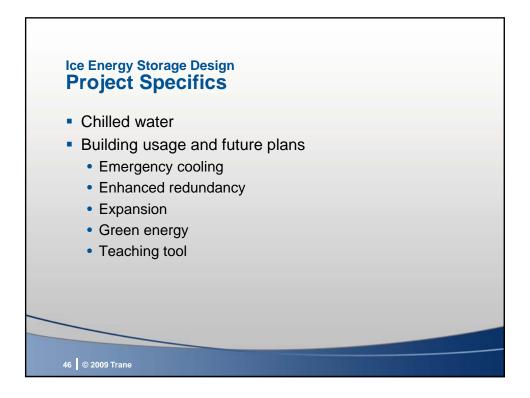














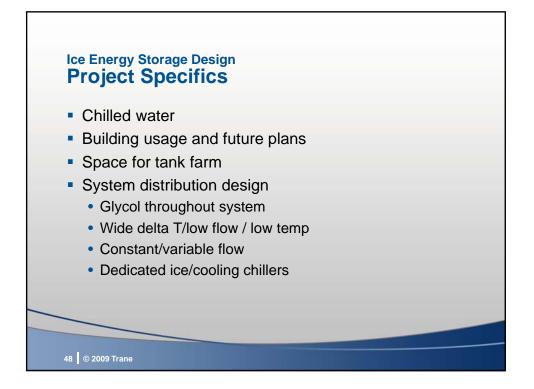
Ice Energy Storage Design **Project Specifics**

- Chilled water
- Building usage and future plans
- Space for tank farm
 - Outside
 - Inside

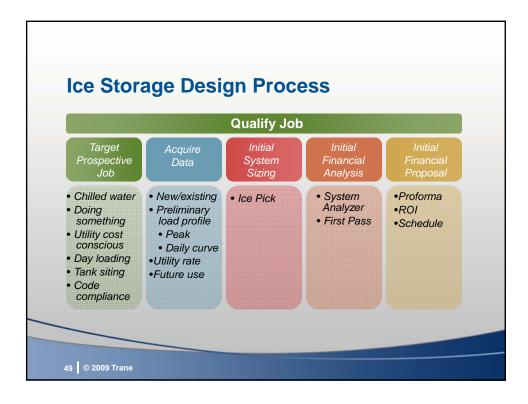
47 © 2009 Trane

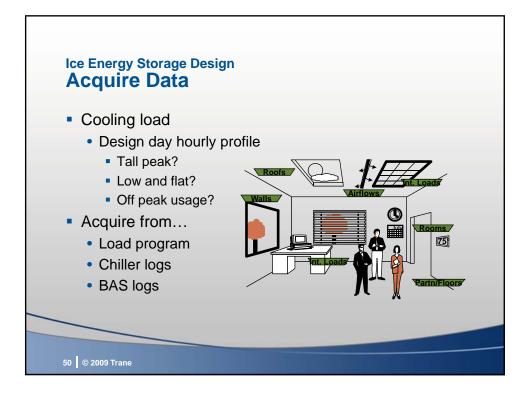
- Stacked
- · Partial or complete burial



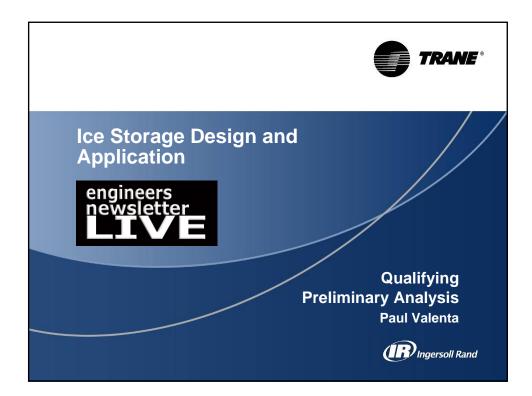


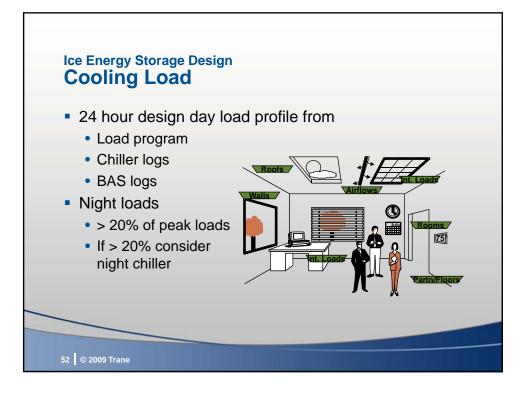




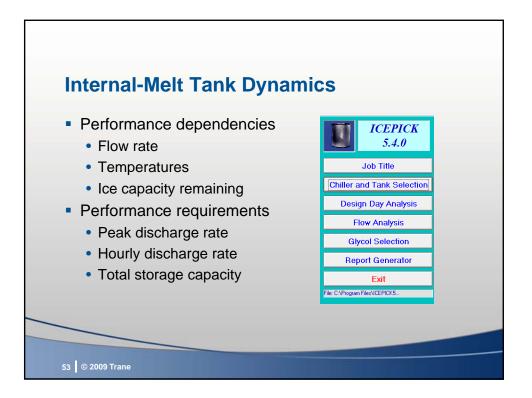


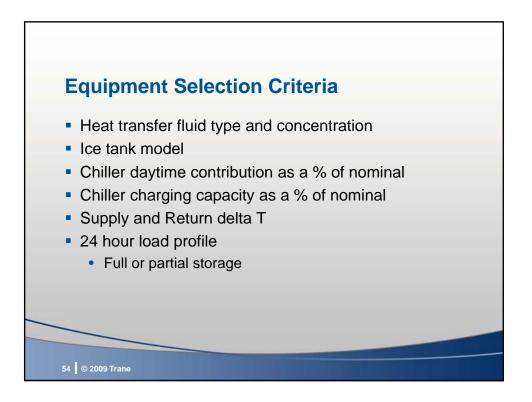










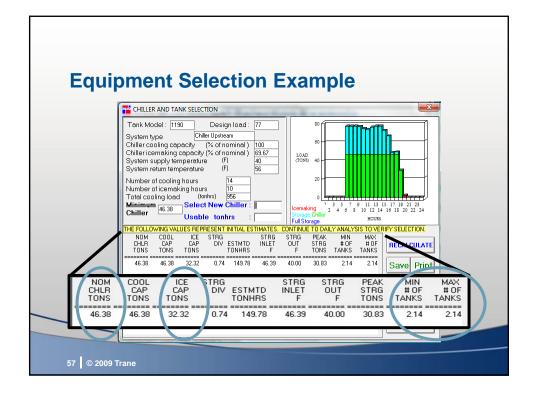


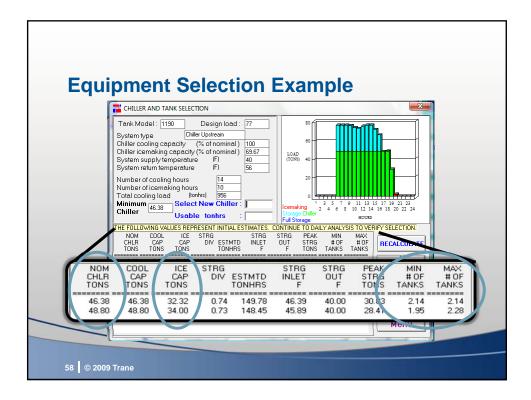


CHILLER AND TANK SELECTION PARAMETERS		
Tank Model	1190	\$
Chiller Cooling Capacity (% of nominal)	100	\$
Chiller Icemaking Capacity (% of nominal)	69.67	*
System Supply Temperature (F)	40	\$
System Return Temperature (F)	56	\$
System Type	Chiller Upstream	-
Menu Help		

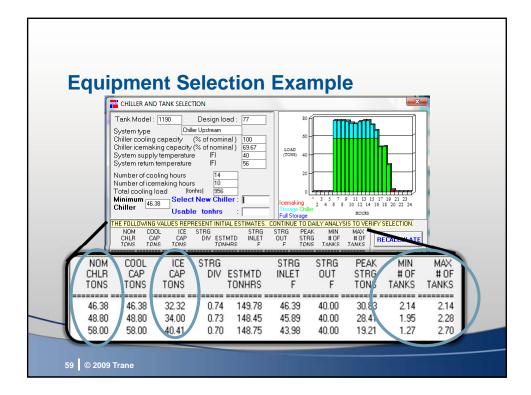
	DESIGN DAY LOAD PRO	Load Pi	iya ke matu	and through the		
н	TONS IOUR LOAD	TYPE CHILLER	% HOUR	TONS	PE_CHILLER %	
	1 0 2 0 3 0 4 0 5 0 6 77.21 9 76.64 10 74.49 11 73.76 12 76.18	• •	 ↓ 14 ↓ 15 ↓ 16 ↓ 17 ↓ 18 ↓ 19 ↓ 20 ↓ 21 ↓ 21 ↓ 22 ↓ 23 	77.21	♦ 83 ♦ ♦ 83 ♦ ♦ 83 ♦ ♦ 83 ♦ ♦ 83 ♦ ♦ 83 ♦ ♦ 83 ♦ ♦ 83 ♦ ♦ 83 ♦ ♦ 83 ♦ ♦ 83 ♦ ♦ 83 ♦ ♦ 69.67 ♦ ♦ 69.67 ♦ ♦ 69.67 ♦ ♦ 69.67 ♦	





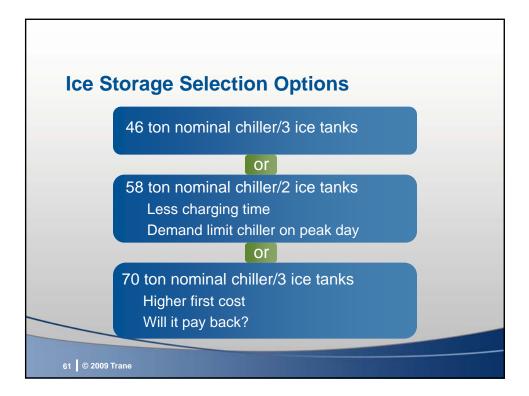


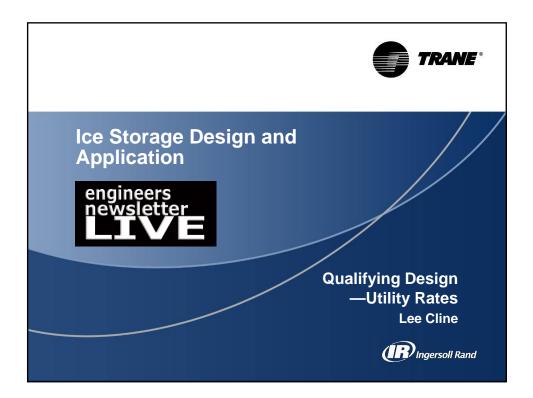




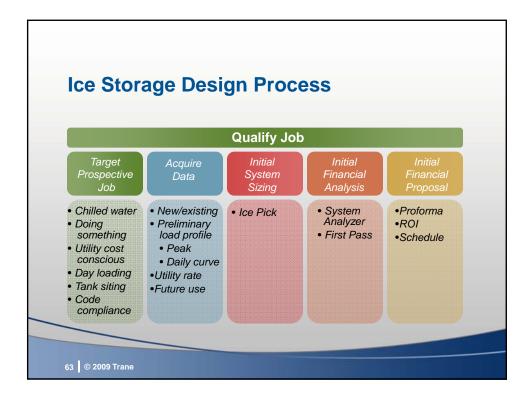
					ysis					
	- L	ATIC E	Y SYSTEM A		ATAL Y	FLOW	DATA		SCHARGE	
IP.				LOAD E		FLUW	DATA	1		
	HOUR	TYPE	LOAL TONS	TONS	TONS	TONS	TOTAL	TONHRS /TANK	PERCENT CHARGE	
	1	I	0	40	40	20	240	120	63.3	
	2	I	0	40 40	40	20	281 321	140	73.9 84.5	
	4	P	0	40	40	20	321	161	84.5	
	5	p	0	0	-29	0	321 292	161	84.5	Hal
	6	p p	77	48	-29	-15	292	146	76.9	Hel
	8	p	77	48	-29	-15	234	117	61.6	
	10	P	74	48	-29	-14	206	90	47.2	Prin
	11	p	74	48	-26	-13	154	77	40.4	
	12	P	76	48	-28	-14	126	63	33.0	Men
	13 14	P	77 77	48 48	-29 -29	-15	96 67	48	25.4 17.7	Men
	15	P	73	48	-25	-12	43	21	11.3	
	16 17	p p	67 49	48 48	-18	-9 0	24 24	12 12	6.4 6.3	🗲
	17	P	49 49	48	-1	-1	24	12	6.3	
	19	P	29	29	0	0	23	11	6.0	
	20 21	I	2	40 40	38 40	19 20	38 79	19 39	10.1 20.7	
	21	I	0	40	40	20	119	39 60	31.4	
	23	I	0	40 40	40 40	20 20	160 200	80 100	42.0	

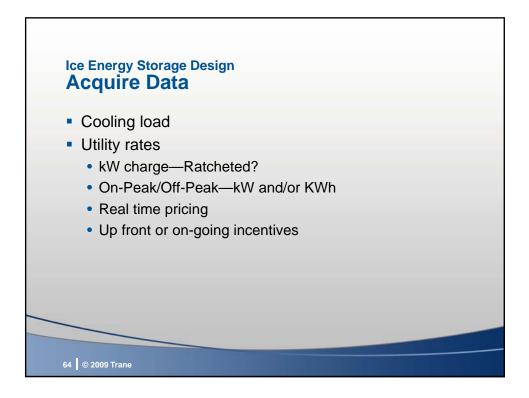




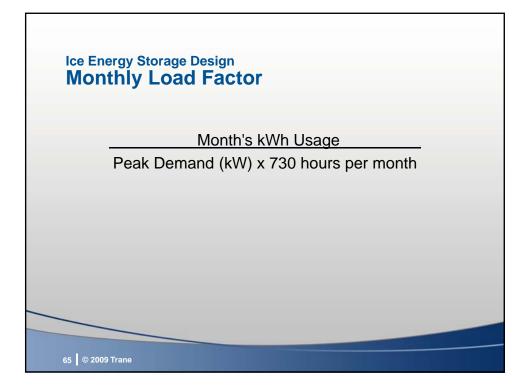


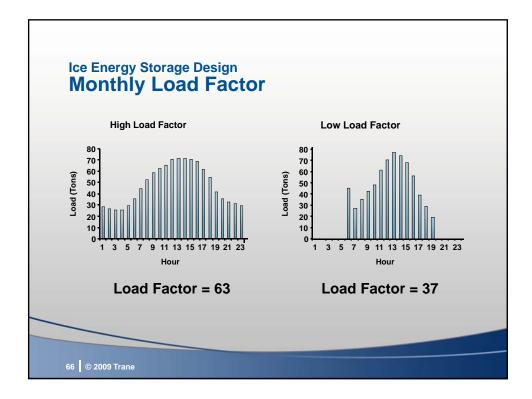




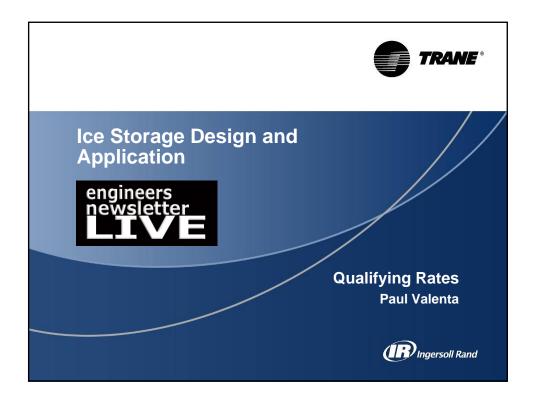


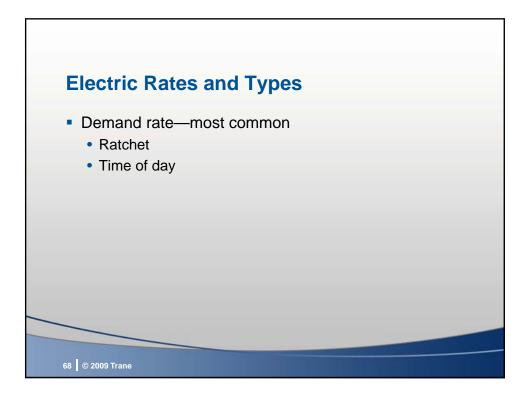




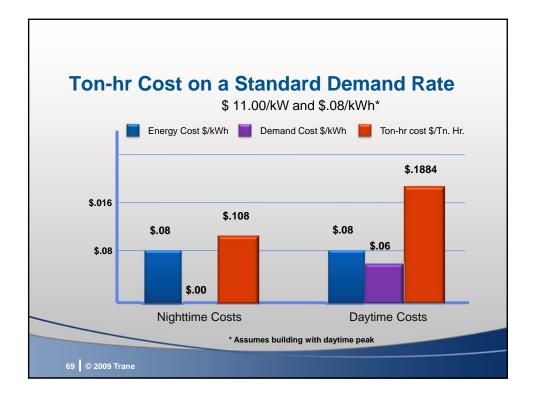


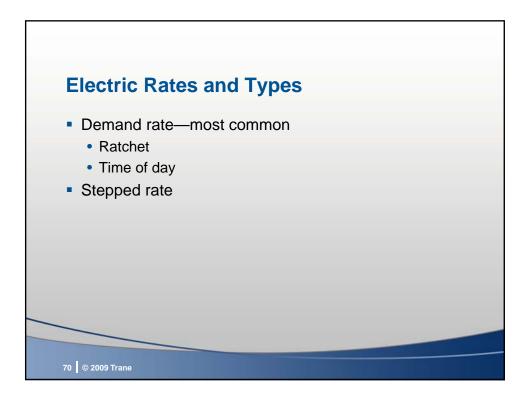




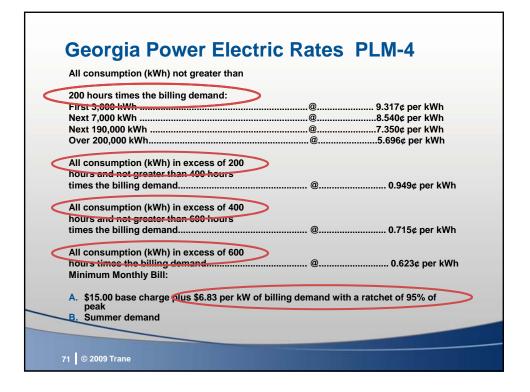


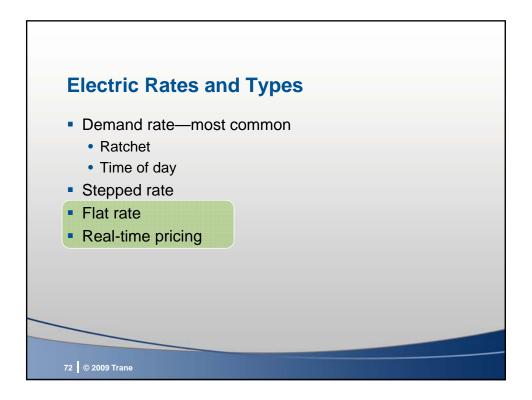




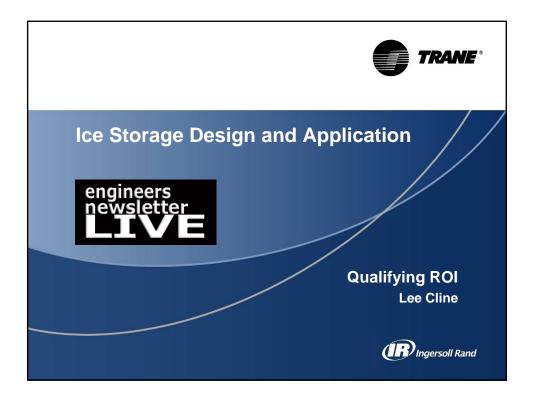


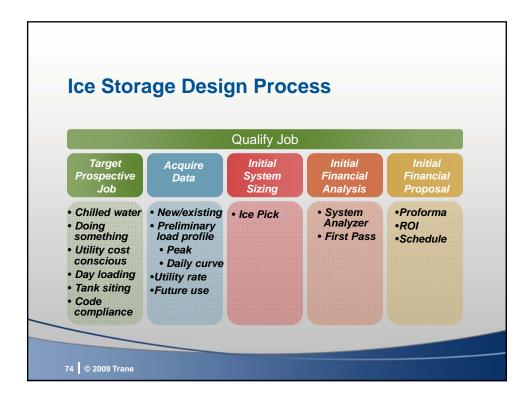






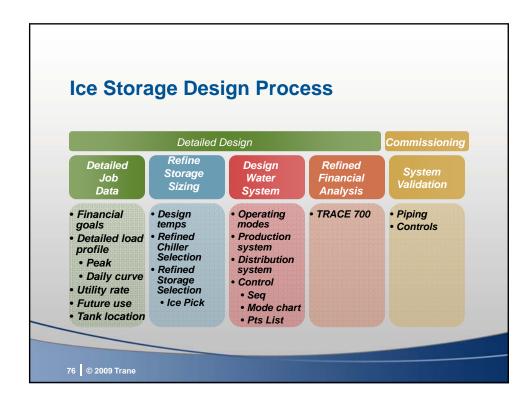




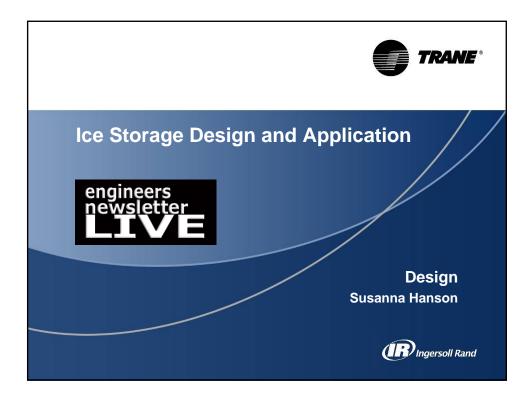


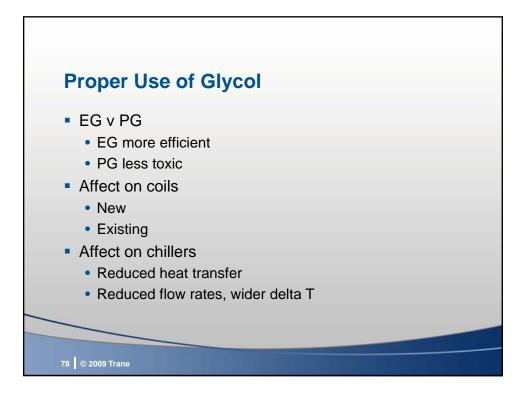






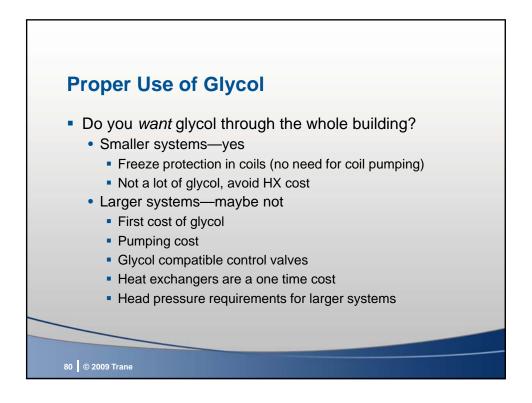








Proper Use	of Glyco	bl	
solution	freeze point	specific heat	viscosity
water	32°F	1.0 Btu/lb-°F	1.5 ср
ethylene glycol (25%)	11.4°F	0.90 Btu/lb-°F	3.2 ср
propylene glycol (30%)	9.3°F	0.92 Btu/lb-°F	5.2 ср
	fluid temper	ature = 40°F	
79 © 2009 Trane			





Prope solution	entering fluid	coil	total capacity MBh		flow rate	pressure drop (fluid) ft. H ₂ O
water	45	6	455	0.64	75.5	6.89
25% EG	45	6	395	0.62	86.4	7.83
81 © 2009 T	rane					

solution		rows		in. H ₂ O	gpm	pressure drop (fluid ft. H ₂ O
water 25% EG	45 45	6 6	455 395	0.64 0.62	75.5 86.4	6.89 7.83
25% EG	45	8	455	0.83	86.4	9.81

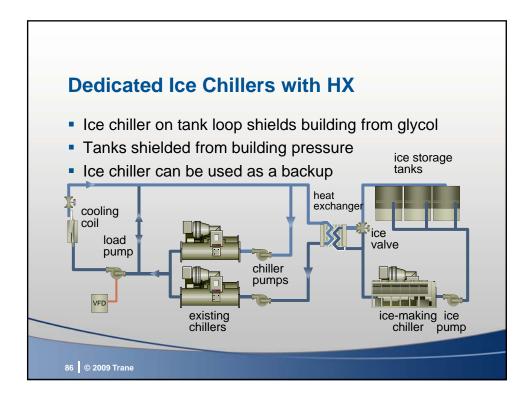


Prope	entering		total		fluid	pressure
solution	fluid °F	coil rows		drop (air) in. H ₂ O		drop (fluid) ft. H ₂ O
water	45	6	455	0.64	75.5	6.89
25% EG	45	6	395	0.62	86.4	7.83
25% EG	45	8	455	0.83	86.4	9.81
25% EG	45	6	455	0.65	120.7	14.3
25% EG	45	6	455	0.65	120.7	14.3

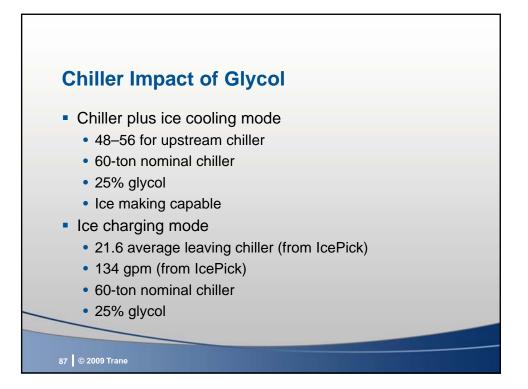
solution	entering fluid °F	coil	total capacity MBh			pressure drop (fluid) ft. H ₂ O
water	45	6	455	0.64	75.5	6.89
25% EG	45	6	395	0.62	86.4	7.83
25% EG	45	8	455	0.83	86.4	9.81
25% EG	45	6	455	0.65	120.7	14.3
25% EG	40	6	455	0.64	84.1	7.52



гор		OI G		-Coils		
	entering fluid	coil	total capacity	pressure drop (air)	fluid flow rate	pressure drop (fluid)
solution	°F	rows		in. H ₂ O		ft. H ₂ O
water	45	6	455	0.64	75.5	6.89
25% EG	45	6	395	0.62	86.4	7.83
25% EG	45	8	455	0.83	86.4	9.81
25% EG	45	6	455	0.65	120.7	14.3
25% EG	40	6	455	0.64	84.1	7.52
25% EG	38	6	455	0.64	76.8	6.41



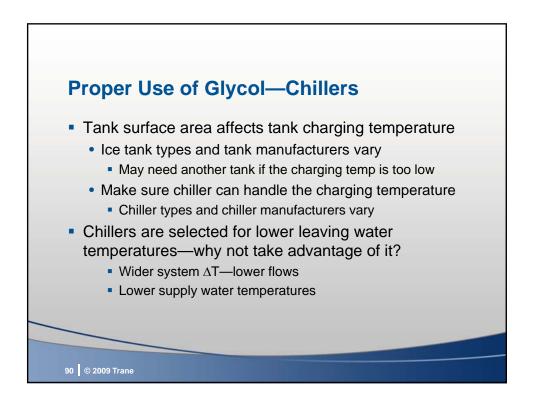




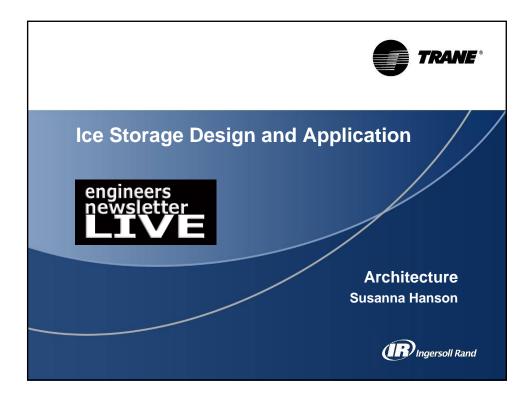
Chiller Se		Dual Modes	
	CGAN	4-1, 48-56	
erformance	CON	11, 10 50	
Unit type: Unit nominal tonnage: Capacity:	High efficiency 60 tons 59.50 tons	Full load efficiency: IPLV: NPLV:	10.7 EER 15.8 EER 16.8 EER
Vaporator Evap application: Evap leaving temp: Evap entering temp: Evap flow rate:	Ice making w/ interface 48.00 F 56.00 F 190.70 gpm	Evap fluid freeze point: Evap fouling factor: Min evap flow rate: Press drop at min evap flow:	11.40 F 0.00010 hr-ft?-deg F/Bt 71.00 gpm 5.70 ft H20
Evap press drop: Evap fluid type: Evap fluid concentration:	35.70 ft H2O Ethylene glycol 25.00 %	Max evap flow rate: Press drop at max evap flow: Pressure vessel code:	213.10 gpm 43.90 ft H2O BPHE - exempt from ASM

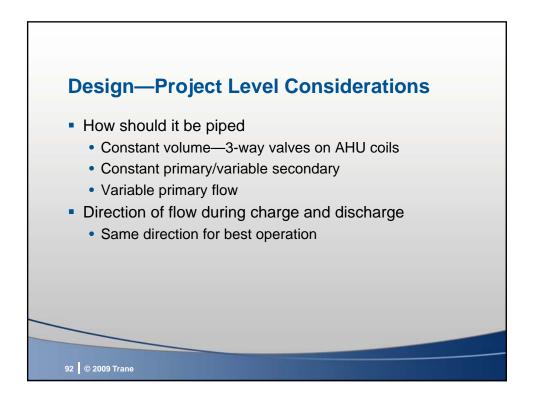


	CGAM	21-27 EG	
erformance			and the second second
Unit type:	High efficiency	Full load efficiency:	7.1 EER
Unit nominal tonnage:	60 tons	IPLV:	15.8 EER
Capacity:	39.60 tons	NPLV:	11.6 EER
vaporator			
Evap application:	Ice making w/ interface	Evap fluid freeze point:	11.40 F
Evap leaving temp:	21.60 F	Evap fouling factor:	0.00010 hr-ft?-deg F/Btu
Evap entering temp:	27.60 F	Min evap flow rate:	71.00 gpm
Evap flow rate:	170.40 apm	Press drop at min evap flow:	5.70 ft H20
Evap press drop:	29.00 ft H20	Max evap flow rate:	213.10 gpm
Evap fluid type:	Ethylene glycol	Press drop at max evap flow:	43.90 ft H20
Evap fluid concentration:	25.00 %	Pressure vessel code:	BPHE - exempt from ASME

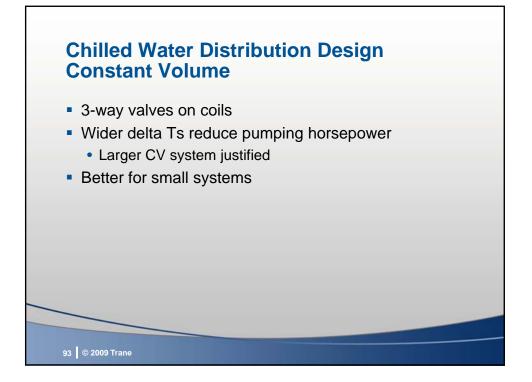


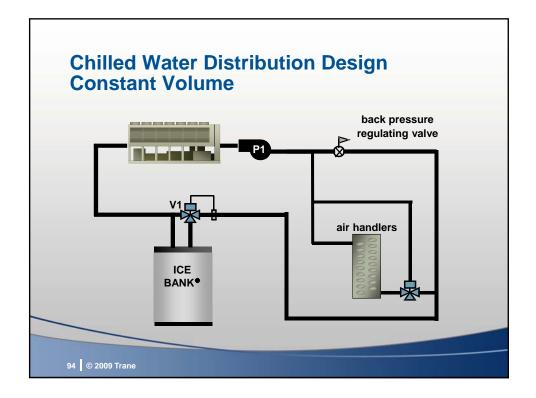




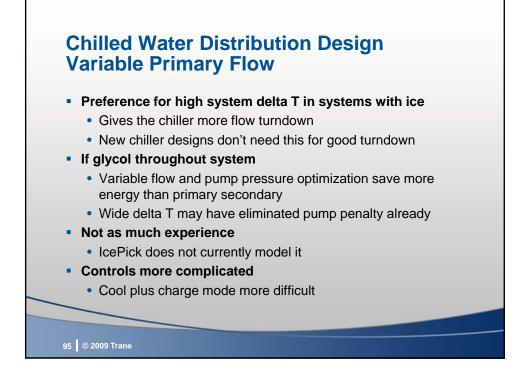


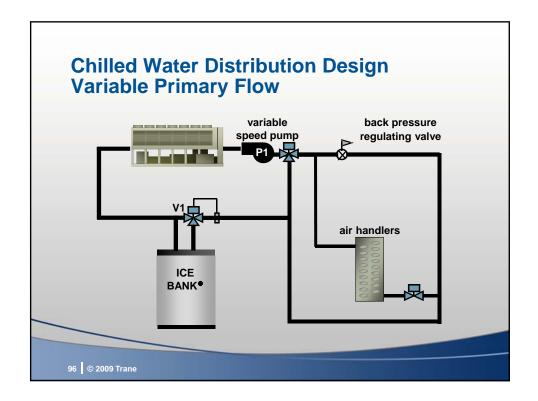




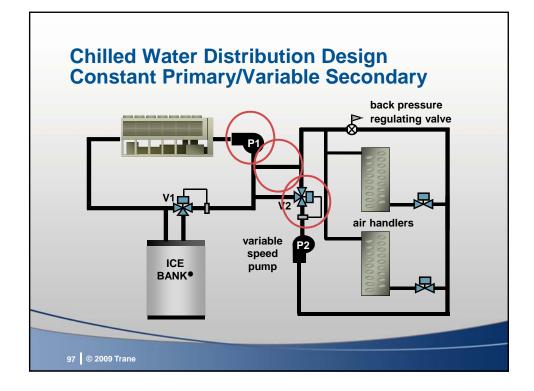


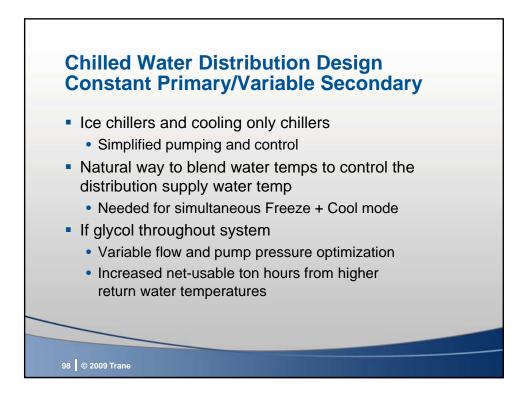




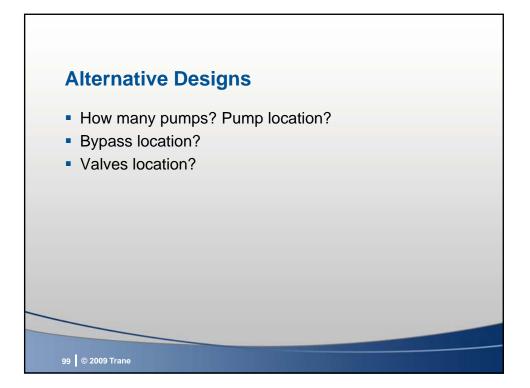


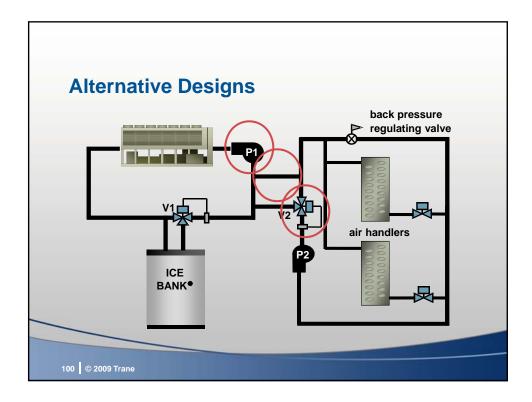




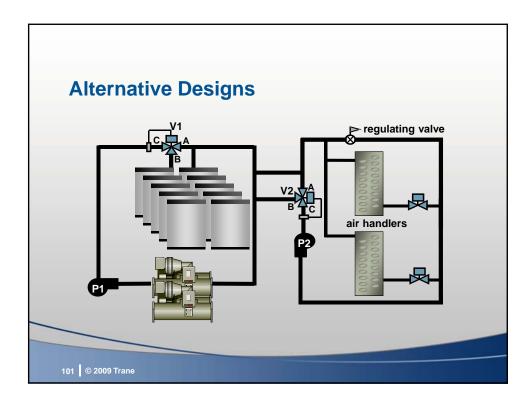


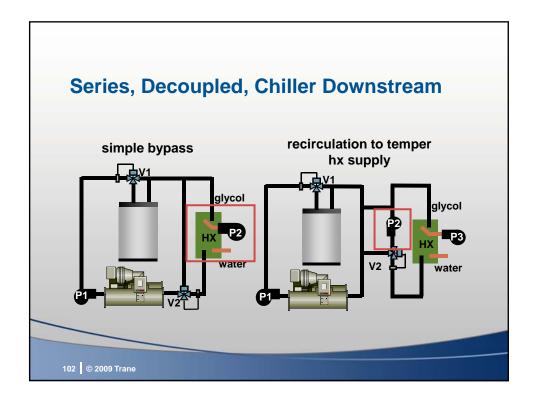




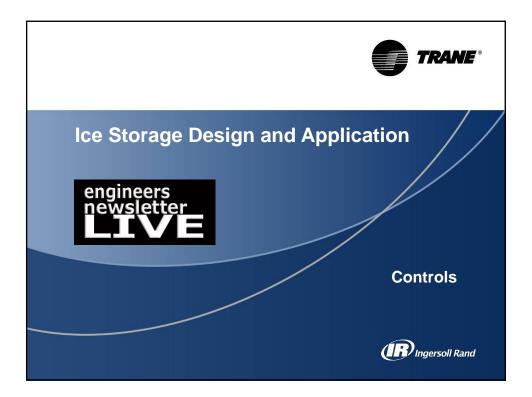


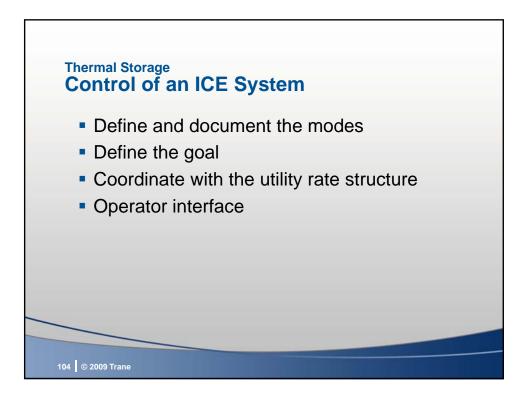




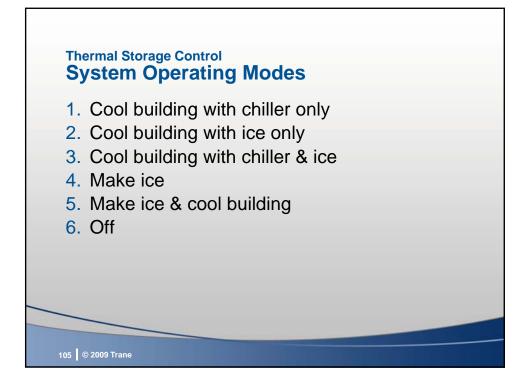


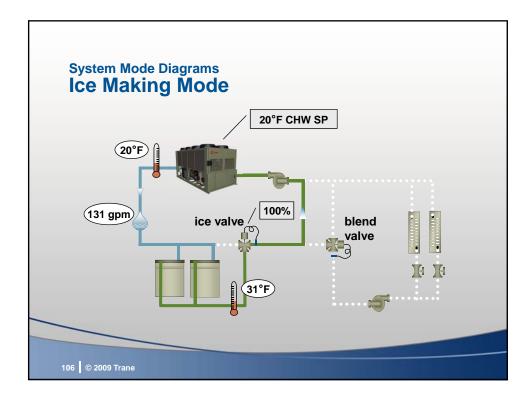




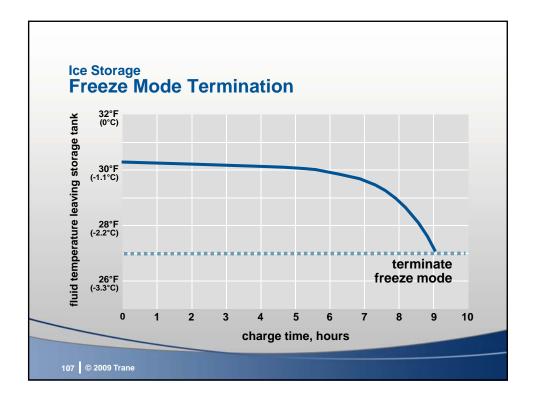


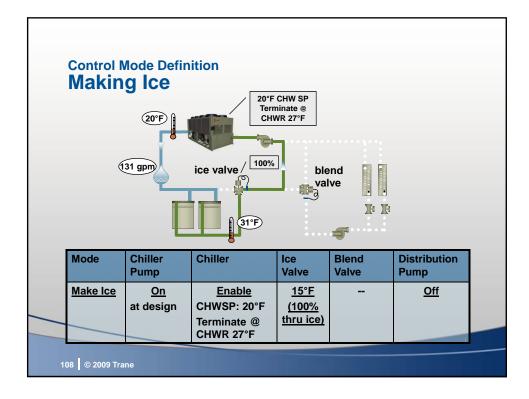




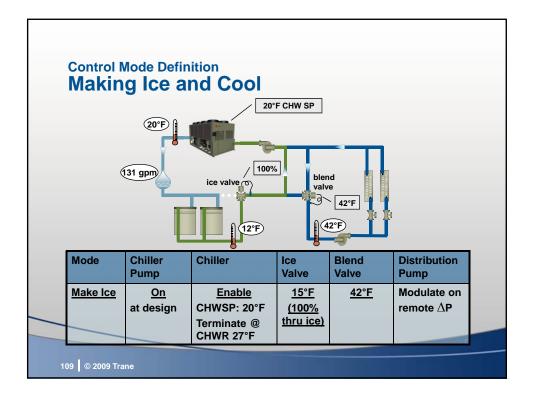


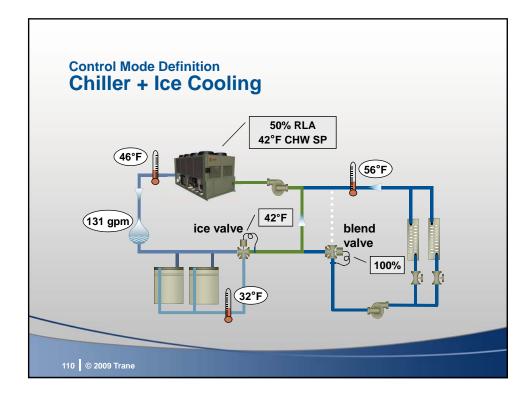




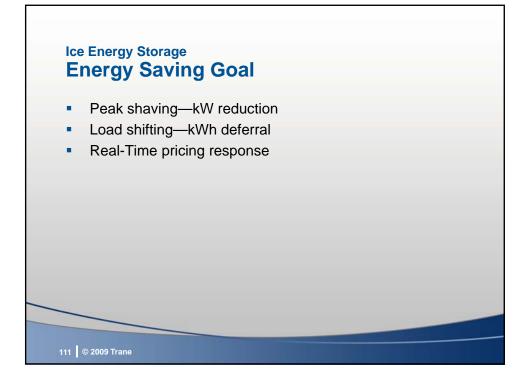


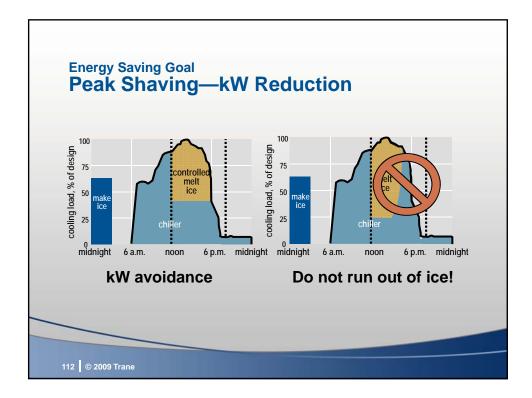




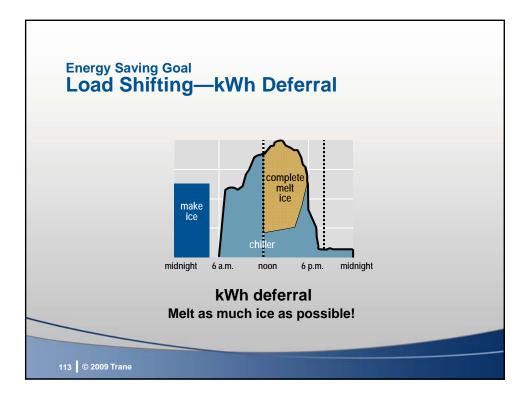


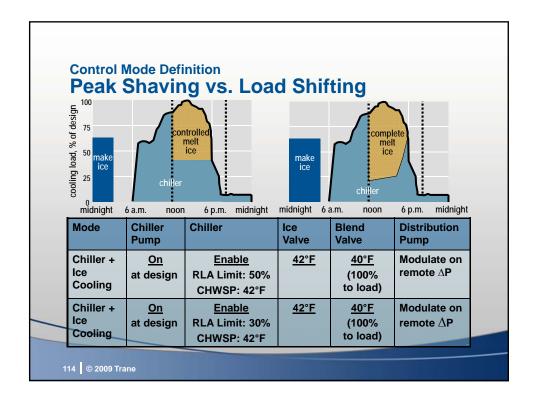






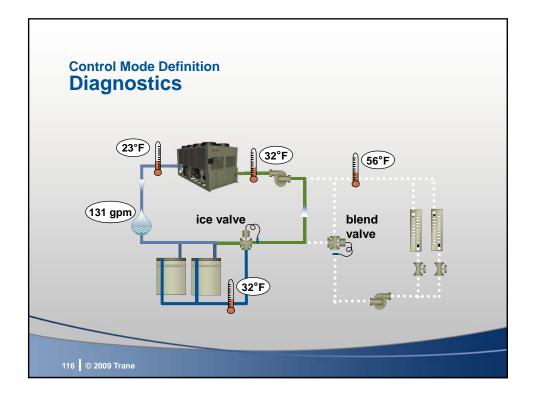




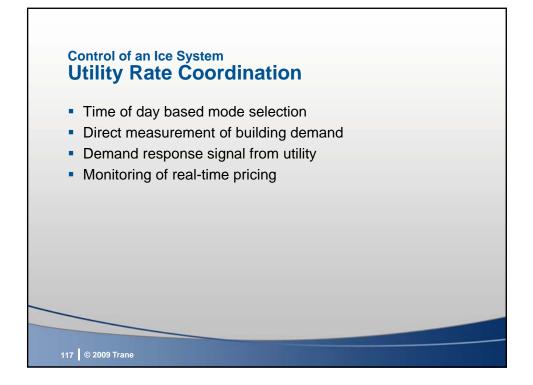


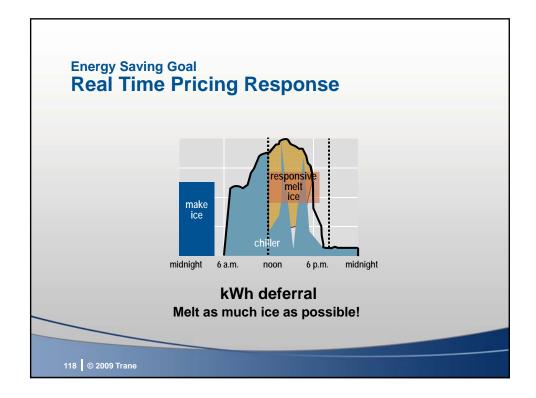


		de Defin			
Mode	Chiller Pump	Chiller	lce Valve	Blend Valve	Distribution Pump
Chiller Only	On	Enable CHWSP 42°F	55°F (0% lce)	40°F (100% to load)	Modulate on remote ∆P
lce Only	On	OFF	42°F	40°F (100% to load)	Modulate on remote ∆P
Chiller & Ice	On	Enable CHWSP 42°F RLA Limit 30-50%	42°F	40°F (100% to load)	Modulate on remote ∆P
Make Ice	On	Enable CHWSP 23°F	15°F (100% to ice)	80°F 0% to load)	Off
Make Ice & Cool	On	Enable CHWSP 23°F	15°F (100% to ice)	42°F	Modulate on remote ∆P
Off	Off	Off	-	-	Off

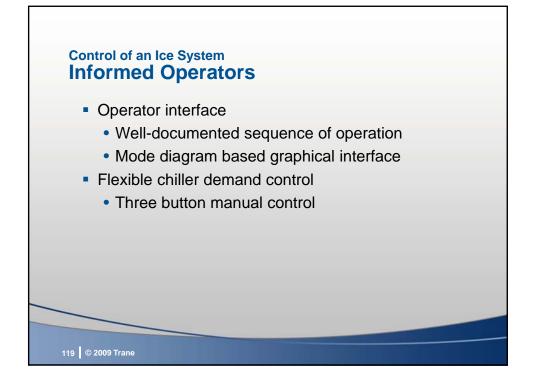


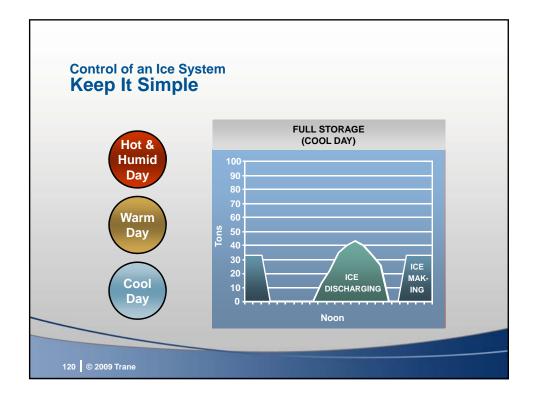




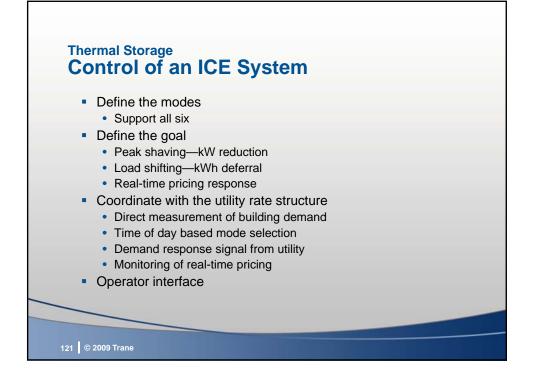


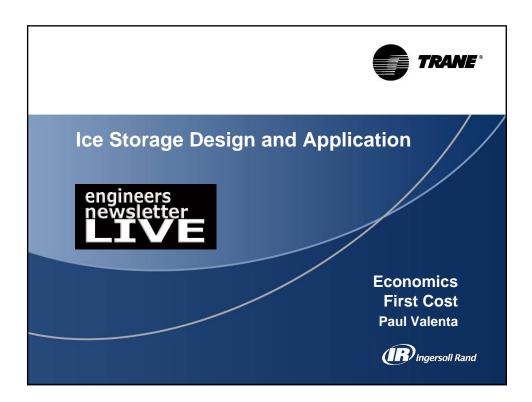




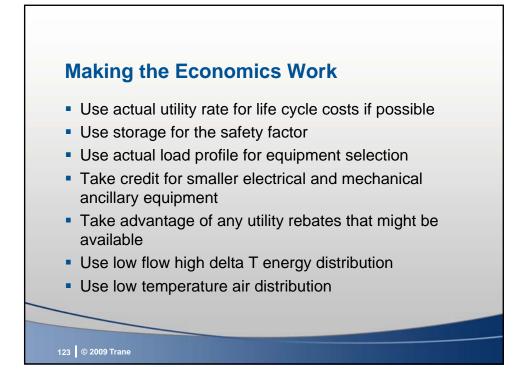








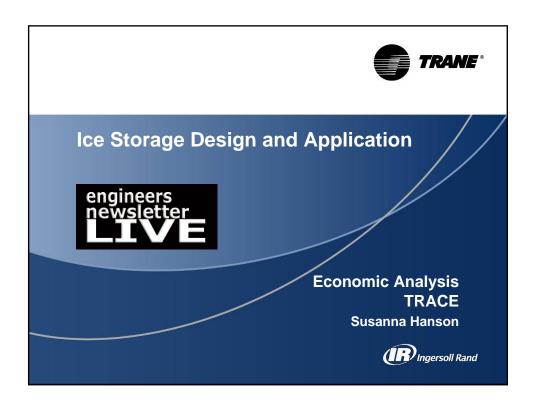




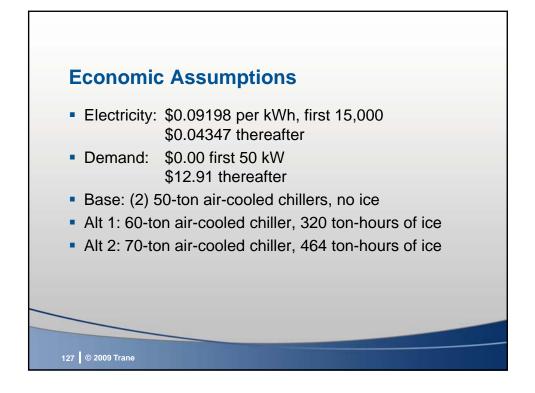


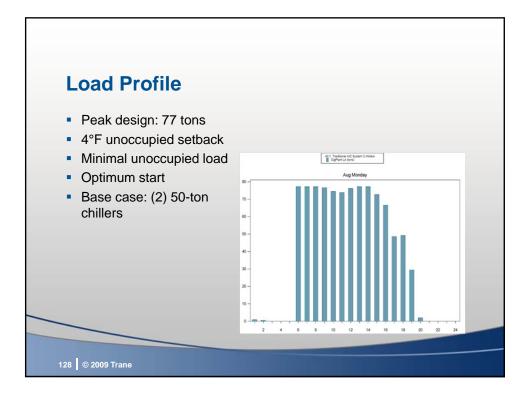


	gional Service C	
	Conventional A/C System	Energy Storage
Chillers	\$717,000	\$447,000
Ice Storage	\$0	\$357,000
Pipe & Pumps	\$ 395,000	\$264,000
Air Distribution	\$ 988,000	\$976,000
TOTAL COST	\$ 2,100,000	\$2,044,000
FPL Rebate	\$0	\$187,500
NET Cost to Customer	\$ 2,100,000	\$1,856,500
Net Cost/Ton	\$2,800	\$2,475
Net First Cost Savings		\$ 243,500
Annual Savings over pas	st 3 years	
Electricity (Demand & Er	nergy)	\$119,500
Maintenance & Water (no	cooling towers)	\$25,000
Total Annual Operating	Savings	\$144,500

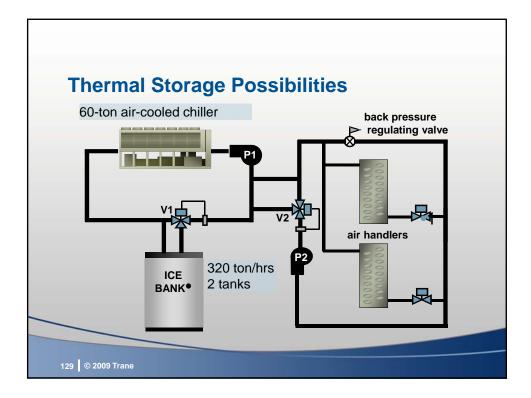


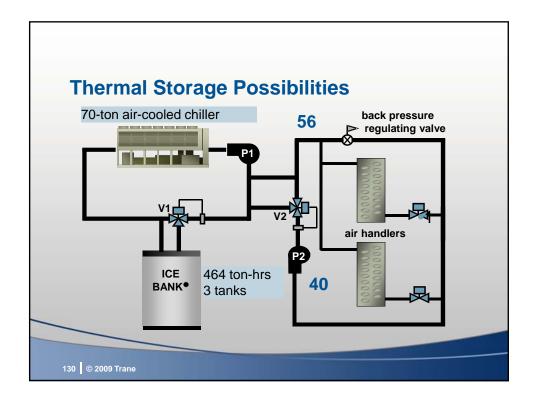


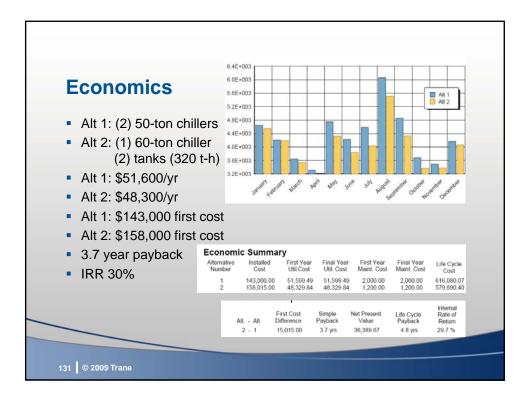


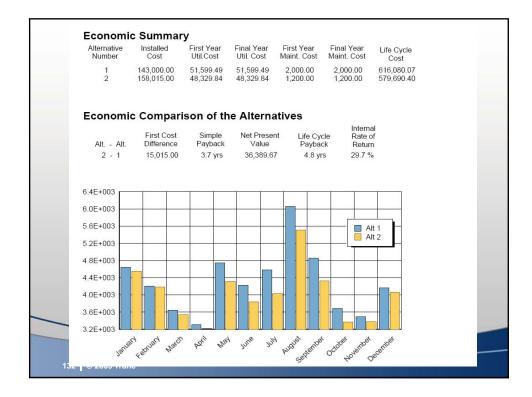






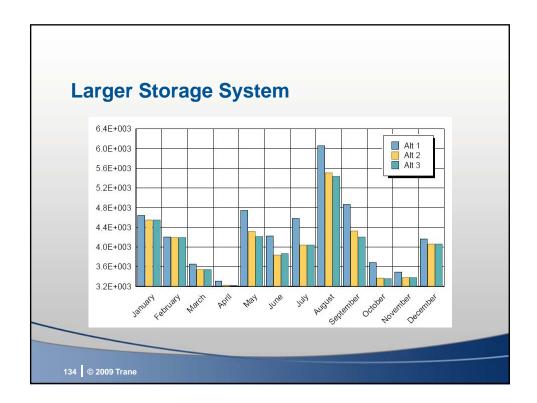








Reduced De	mand			
Alternative 1 Yearly Time of Peak: 14(Hr) 8(M	Traditional A/C S	ystem 2 cl		
Equipment Description			Electrical Demand (kw)	Percent of Total (%)
Cooling Equipment Air-cooled chiller - 002 Air-cooled chiller - 001			61.68 68.88	27.72 30.95
	-	Sub total	130.56	58.67
Alternative 3 Yearly Time of Peak: 11(Hr) 8	Larger Therma	I Storage	1 c	
Equipment Description			Electrical Demand (kw)	Percent of Tota (%)
Cooling Equipment Air-cooled chiller - 001			59.54	36.46
	-	Sub total	59.54	36.46





Larger Storage System • Lower kW • About the same kWh • 11 year payback versus no storage, 10.5% IRR • Smaller storage system better Economic Summary <u>Alternative loss</u> <u>Installed Cost Util Cost Util Cost Willi Cost Waint. Cost Maint. C</u>							
 About the same kWh 11 year payback versus no storage, 10.5% IRR Smaller storage system better Economic Summary Alternative Installed Cost Installed Vill.Cost Installed Villl.Cost I	Largei	r Stora	ge Sys	stem			
 11 year payback versus no storage, 10.5% IRR 5 Smaller storage system better <i>Economic Summary</i> Alternative Installed Cost <i>First Year Final Year Maint. Cost</i> <i>High and Cost</i>	Lower	kW					
• Smaller storage system better Economic Summary Alternative Installed First Year Final Year Final Year Final Year 1 143,000.00 51,599.49 51,599.49 2,000.00 2,000.00 2,000.00 2 158,015.00 48,329.84 48,329.84 1,200.00 1,200.00 1,200.00 3 193,023.00 48,035.53 48,035.53 1,200.00 1,200.00 1,200.00 Economic Comparison of the Alternatives Internal Rate of Return Internal Rate of Return Rate of Return Alt Alt. First Cost Simple Net Present Value Life Cycle Rate of Return 2 - 1 15,015.00 3.7 yrs 36,389.67 4.8 yrs 29.7 % 3 - 1 50,023.00 11.5 yrs 3,887.36 15 1 yrs 10.9 %	About	the same I	‹ Wh				
• Smaller storage system better Economic Summary Alternative Installed First Year Final Year Final Year Final Year 1 143,000.00 51,599.49 51,599.49 2,000.00 2,000.00 1,200.00 2 158,015.00 48,329.84 48,329.84 1,200.00 1,200.00 1,200.00 3 193,023.00 48,035.53 48,035.53 1,200.00 1,200.00 1,200.00 Economic Comparison of the Alternatives Internal Rate of Return Internal Rate of Return Rate of Return 4.t Alt. First Cost Simple Net Present Value Life Cycle Rate of Return 2 - 1 15,015.00 3.7 yrs 36,389.67 4.8 yrs 29.7 % 3 - 1 50,023.00 11.5 yrs 3,887.36 15 1 yrs 10.9 %	11 vea	r pavback	versus no	storage.	10.5% IF	R	
Economic Summary Alternative Number Installed Cost First Year Util. Cost Final Year Util. Cost First Year Maint. Cost Final Year Maint. Cost Life Cycle Cost 1 143,000.00 51,599.49 51,599.49 2,000.00 2,000.00 2,000.00 2,000.00 1,200.00 1,200.00 1,200.00 1,200.00 1,200.00 1,200.00 616,080.07 57,690.40 612,192.71 Economic Comparison of the Alternatives Alt Alt. First Cost Difference Simple Payback Net Present Value Life Cycle Payback Internal Rate of Return 2 1 15,015.00 3,7 yrs 36,389.67 4.8 yrs 29.7 % 3 1 50,023.00 11.5 yrs 3,887.36 15 1 yrs 10.9 %	•			•			
Alternative Number Installed Cost First Year Util.Cost Final Year Util.Cost First Year Maint. Cost Final Year Maint. Cost Life Cycle Cost 1 143,000.00 51,599.49 51,599.49 2,000.00 2,000.00 2,000.00 1,200.00 2 158,015.00 48,329.84 48,329.84 1,200.00 1,200.00 1,200.00 1,200.00 3 193,023.00 48,035.53 48,035.53 1,200.00 1,200.00 1,200.00 612,192.71 Economic Comparison of the Alternatives Alt Alt. First Cost Difference Simple Payback Net Present Value Life Cycle Payback Internal Rate of Return 2 - 1 15,015.00 3.7 yrs 36,389.67 4.8 yrs 29.7 % 3 - 1 50,023.00 11.5 yrs 3,887.36 15 1 yrs 10.9 %		U U	•				
Number Cost Util.Cost Util. Cost Maint. Cost Maint. Cost Cost 1 143,000.00 51,599.49 51,599.49 2,000.00 2,000.00 616,080.07 2 158,015.00 48,329.84 48,329.84 1,200.00 1,200.00 612,192.71 Economic Comparison of the Alternatives Alt Alt. First Cost Simple Payback Net Present Value Life Cycle Payback Internal Rate of Return 2 1 15,015.00 3.7 yrs 36,389.67 4.8 yrs 29.7 % 3 1 50,023.00 11.5 yrs 3,887.36 15 1 yrs 10.9 %	Economic	: Summary					
2 158,015.00 48,329.84 48,329.84 1,200.00 1,200.00 579,690.40 3 193,023.00 48,035.53 48,035.53 1,200.00 1,200.00 612,192.71 Economic Comparison of the Alternatives Alt Alt. Difference Payback Net Present Life Cycle Rate of Return 2 - 1 15,015.00 3.7 yrs 36,389.67 4.8 yrs 29.7 % 3 - 1 50,023.00 11.5 yrs 3,887.36 15 1 yrs 10.9 %							
First Cost Simple Net Present Life Cycle Internal Alt Alt. Difference Payback Value Payback Return 2 - 1 15,015.00 3.7 yrs 36,389.67 4.8 yrs 29.7 % 3 - 1 50,023.00 11.5 yrs 3,887.36 15 1 yrs 10.9 %		158,015.00	48,329.84	48,329.84	1,200.00	1,200.00	579,690.40
First CostSimple PaybackNet Present ValueLife Cycle PaybackRate of Return2 - 115,015.003.7 yrs 3 - 136,389.674.8 yrs 15,023.0029.7 % 10.9 %	Economic	: Comparis	on of the <i>i</i>	Alternative	es		
- 3 - 1 50,023.00 11.5 yrs 3,887.36 <u>15.1 yrs</u> 10.9 %	Alt Alt.						Rate of
	3 - 1	50,023.00	11.5 yrs	3,887.36	15.1	/rs	10.9 %
3 - 2 35,008.00 118.9 yrs -32,502.31 Does not pay back Does not pay back	3 - 2	35,008.00	118.9 yrs	-32,502.31	Does not p	ay back Does	s not pay back

Alternative 1 Yearly Time of Peak: 14(Hr)	Traditional A/C 8(Month)	C System 2 cl		
Equipment Description			Electrical Demand (kw)	Percent of Total (%)
Cooling Equipment Air-cooled chiller - 002 Air-cooled chiller - 001			61.68 68.88	27.72 30.95
		Sub total	130.56	58.67
Alternative 2	Thermal Stora	ge 1 chiller 2		
Yearly Time of Peak: 11(Hr)	8(Month)			
Equipment Description			Electrical Demand (kw)	Percent of Total (%)
Cooling Equipment Air-cooled chiller - 001			69.86	40.23
		Sub total	69.86	40.23
Alternative 3	Larger Therr	nal Storage	1 c	
Yearly Time of Peak: 11(Hr) 8(Month)			
Equipment Description			Electrical Demand (kw)	Percent of Tota (%)
Cooling Equipment Air-cooled chiller - 001			59.54	36.46
		Sub total	59.54	36.46



We Go ic Summa Installed Cost 143,000.00 146,015.00		Final Year			
ic Summa Installed Cost 143,000.00 146,015.00	ry First Year Util.Cost	Final Year			
ic Summa Installed Cost 143,000.00 146,015.00	ry First Year Util.Cost	Final Year			
Installed Cost 143,000.00 146,015.00	First Year Util.Cost				
Installed Cost 143,000.00 146,015.00	First Year Util.Cost				
146,015.00	51 599 49	Util. Cost	First Year Maint. Cost	Final Year Maint. Cost	Life Cycle Cost
179,023.00	48,329.84 48,035.53	51,599.49 48,329.84 48,035.53	2,000.00 1,200.00 1,200.00	2,000.00 1,200.00 1,200.00	616,080.07 567,690.40 598,192.71
ic Compa	rison of t	he Altern	atives		
					nternal
First Cost Difference	Simple Payback	Net Present Value	Life Cyc Paybac		Rate of Return
3,015.00	0.7 yrs	48,389.67	0.8 yrs		35.0 %
36.023.00	8.3 vrs	40,309.07	14.2 yr		5.0 %
33,008.00	112.2 yrs	-30,502.31		yback Doesn	
c Compari	son of th	e Alterna	tives		
•				Ir	nternal
First Cost Difference	Simple Payback	Net Present Value	Life Cyc Paybac		Rate of Return
3,015.00	0.4 yrs	75,417.46			40.3 %
		· · ·	, , , , , , , , , , , , , , , , , , , ,		5.0 %
22,000,00	20.3 yrs	-22,305.90	Does not pa	iy back. Does n	ограу раск
	3,015.00 36,023.00 33,008.00	36,023.00 4.2 yrs	36,023.00 4.2 yrs 53,111.56	36,023.00 4.2 yrs 53,111.56 5.8 yrs	36,023.00 4.2 yrs 53,111.56 5.8 yrs 2

